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In re Patent Application of

Dally MOYA et al.

Application No.: ~~New Application~~ 09/917674

Filed: July 31, 2001

For: (METH)ACRYLIC ESTER BINDERS
FROM GLYCOLYZED AROMATIC
POLYESTERS

Group Art Unit: ~~Unassigned~~ 1713

Examiner: ~~Unassigned~~

Zalukac

1c971 U.S. PTO
09/917674
07/31/01

CLAIM FOR CONVENTION PRIORITY

Assistant Commissioner for Patents
Washington, D.C. 20231

Sir:

The benefit of the filing date of the following prior foreign application in the following foreign country is hereby requested, and the right of priority provided in 35 U.S.C. § 119 is hereby claimed:

European Patent Application No. 00116565.3

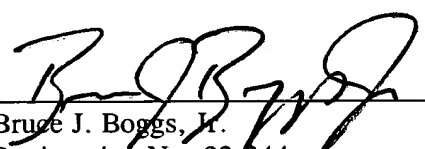
Filed: August 1, 2000.

In support of this claim, enclosed is a certified copy of said prior foreign application. Said prior foreign application was referred to in the oath or declaration. Acknowledgment of receipt of the certified copy is requested.

Respectfully submitted,

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are exact copies of the
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Patentanmeldung Nr. Patent application No. Demande de brevet n°

00116565.3

Der Präsident des Europäischen Patentamts;
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For the President of the European Patent Office

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**Blatt 2 der Beschreibung
Sheet 2 of the certificate
Page 2 de l'attestation**

Anmeldung Nr.:
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Anmelder:
Applicant(s):
Demandeur(s):
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Bezeichnung der Erfindung:
Title of the invention:
Titre de l'invention:
(Meth) acrylic ester binders from glycolized aromatic polyesters

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(Meth)acrylic ester binders from glycolyzed
aromatic polyesters

5 Technical Field

The present invention relates to low-cost (meth)acrylic ester binders and such binder comprising compositions, the synthesis of such binders starting from polyesters such as polyethylene terephthalate (PET), and
10 their application in reactive acrylic systems, particularly in adhesives, coatings and floorings.

Background of the invention

15 The use of polyesters, in particular PET, in film and fiber applications has increased drastically in the past several years. According to the Sherwin-Williams patent US 5 252 615, PET accounted for about 20 % by volume of the world's solid waste in 1993. A large amount of
20 scrap and waste materials is still resulting from the production and consumption of PET every year and therefore, processes which can make use of recycled PET are economically interesting. Taking into account that environmental care and ecological balance have a high priority for the chemical industry today, the conversion of
25 PET waste and scraps into usable raw materials is a continuous challenge. Besides reducing waste, the use of recycled plastics contributes also to the ecological compatibility of commercial products.

30 Several methods have been developed for converting PET into aromatic polyester polyols which are valuable, and low-cost raw materials for the production of adhesive, coating and flooring compositions.

Adhesives, coatings and floorings have to
35 fulfill several requirements in order to be considered for industrial applications. Preferably, the compositions should combine a long open time with a fast curing speed.

The cured systems should exhibit good mechanical and adhesive properties, besides high weather and chemical resistance. However, not only the technical requirements but also the economical aspects determine the choice of adhesives, coatings and floorings for industrial applications. The price of a composition depends mainly on the costs of its reactive components, therefore, it is important to reduce the costs of said reactive components as much as possible. Processes which make use of inexpensive starting materials such as PET allow the production of low-cost components for adhesives, coatings and flooring compositions.

For industrial applications of such compositions, high speed in curing, especially at room temperature, is advantageous, particularly in manufacturing operations where it is expensive to wait until the systems are fully cured. Consequently, compositions with a high curing speed and enough long open time to allow application are desired. One class of systems which can be adapted more readily to fit these requirements is the class of polymerizable acrylate based systems. Acrylic compositions that cure according to a free radical polymerization mechanism reach final strength within minutes at room temperature. This fast strength build-up confers acrylic compositions advantages in comparison to compositions based on epoxies and urethanes which need several hours to reach the same grade of strength.

Methyl methacrylate (MMA) is the most widely used monomer in radically curing acrylic systems. Despite the low cost and excellent properties of this monomer, its strong and disagreeable smell restricts to a great extent its use in adhesive, coating and flooring compositions. All other commercially available low-odor acrylic monomers are expensive, and for that reason novel low-odor/low-cost acrylic monomers which can be used for acrylic systems are needed.

Next to the fast curing, acrylic systems are also known for other advantages like high strength and high chemical resistance to acids and alkalines. A disadvantage of the standard acrylic systems is the relatively high shrinkage. Large shrinkage on curing leaves substantial residual stress which can lead to delamination of a joint. The shrinkage is correlated to the molar mass of the used monomers. For high molar mass oligomers, the relation between the molar mass and the amount of reactive groups is higher, therefore, the shrinkage will be lower. US 3 194 783 describes formulations with high mechanical properties and low shrinkage based on epoxy-acrylates. These oligomers are widely used in compositions for adhesives or floors. But the diacrylate of bisphenol-A diglycidylether is a very high viscous compound, which has to be diluted. The acrylates derived from ethoxylated bisphenol-A diglycidylether have a lower viscosity, but with increasing ethoxylation grade the tensile strength decreases. Moreover, the ethoxylation process is not a simple reaction procedure.

Acrylic compositions, containing cycloaliphatic compounds, with high strength and low shrinkage are described in DE 3 940 138 A1. These cycloaliphatic compounds are unsaturated esters of glycol monodicyclopentenyl ethers and have a low viscosity. But the reaction of dicyclopentadiene with glycols to form this intermediate is very difficult and time consuming.

PU-acrylates, polyurethane prepolymers which are capped with ethylenically unsaturated end groups, are frequently used in acrylic systems and have a low shrinkage. The moderate-to-long chain prepolymers employed, comprise polyether-urethane or polyester-urethane derivatives formed by reacting a polyether or a polyester polyol with a diisocyanate. Polyether based PU-acrylates have low mechanical properties and temperature resistance. Polyester based PU-acrylates have a high viscosity

or are crystalline at room temperature, and show poor compatibility to acrylic monomers.

It is also already known that acrylic ester monomers can be synthesized by direct esterification of
5 (meth)acrylic acid with alcohols in the presence of an acid catalyst, a polymerization inhibitor, and an inert solvent to azeotrope the water formed during reaction. Several syntheses which use polyols as the alcohol component have also been reported. In general, all described
10 processes for the synthesis of acrylic ester monomers from (meth)acrylic acid have the following limitations:
1. use of high cost raw materials and 2. production processes requiring expensive and time consuming reaction work up and product purification.

15 US 3 645 984 reports the preparation of acrylic ester monomers by reacting a diol with (meth)acrylic acid or their anhydrides or acid chlorides. In EP 0 519 410 A2 aromatic polyether alcohols, prepared from aromatic alcohols and ethylene oxide or propylene
20 oxide, are reacted with (meth)acrylic acid to yield novel acrylic ester monomers. In both patent documents, after the esterification has finished, the unreacted (meth)acrylic acid and catalyst are neutralized and the mixtures are washed several times with aqueous solutions.
25 Then, the inert solvent is removed and the acrylic ester monomers are purified by extraction or distillation to separate them from side products and polymerization inhibitor. Besides being time consuming, the washing steps and (meth)acrylate purification cause considerable product loss decreasing the yield of the process.
30

EP 0 126 341 A2 and EP 0 921 168 A1 report processes for the synthesis of (meth)acrylic ester monomers by direct esterification of (meth)acrylic acid with polyester and/or polyether alcohols and polyols, and subsequent reaction with epoxies. According to these documents, the washing steps and purification of end products are avoided by reacting with epoxies the (meth)acrylic

acid remaining in the mixture after esterification. For this purpose, after the esterification has finished, the inert solvent is removed and the esterification catalyst is neutralized. Then, an epoxy amount corresponding to the equivalent acid content of the mixture is added and the reaction is carried out at about 100°C in the presence of a suitable catalyst. Though the end products can be obtained in high yields and can be further used without purification, the reaction with epoxies implies an additional process step. The high temperatures needed for the reaction could also lead to polymerization of the synthesized (meth)acrylates. For the reaction with epoxies, the reaction mixtures must contain a certain amount of (meth)acrylic acid, and, therefore, the direct esterification has to be achieved in the presence of (meth)acrylic acid excess, or additional acid has to be added after esterification.

It is furthermore already known that PET can be used as starting material for the production of polyester polyols useful in reactive polyurethanes compositions. *E.g.* US 4 048 104 relates to polyisocyanate prepolymers, prepared from PET digestion products, which are usable in polyurethane elastomers, adhesives and foams. PU-foams with increased physical strength properties are prepared in US 4 223 068 and US 4 417 001 by replacing a certain amount of the reactive polyol component with a digestion product of PET. Polyester polyol compositions obtained from PET show partial crystallization which lead to low storage stability of the mixtures. EP 0798 325 A1 reports polyhydroxy compounds from PET with increased chemical compatibility, which are suitable for polyurethane syntheses.

Non reactive hot melts and/or pressure-sensitive adhesives have also been prepared using PET based polyester polyols. US 5 008 366 and US 3 993 629 disclose polyester based compositions using polyesters obtained from PET. An adhesive or coating composition

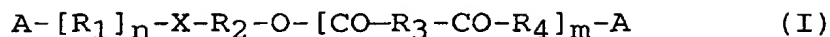
which comprises a reaction product of PET polyester with a difunctional organic acid is reported in WO 95/21213.

EP 0 558 905 A1 describes the preparation of non reactive, physically drying aqueous coating compositions from (optionally waste) PET. The polyethylene terephthalate is first reacted with an alcohol and then with carboxylic acids or their anhydrides to form low-molecular-weight polyesters which can be further subjected to direct acrylic modification. Direct acrylic modification is typically conducted under conditions described in US 4 735 995 and US 4 873 281. The low-molecular-weight polyesters which may contain reactive double bonds are reacted in the presence of organic solvents and ethylenically unsaturated vinyl monomers after a free radical polymerization. Direct acrylic modification means in this case copolymerization with acrylic monomers and not functionalization of the polyester to obtain polymerizable acrylic ester monomers for radically curing acrylic systems.

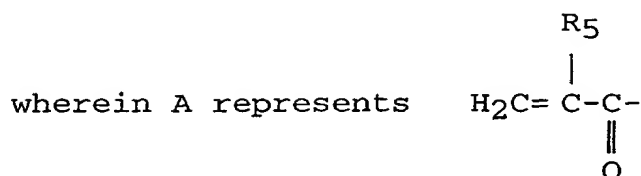
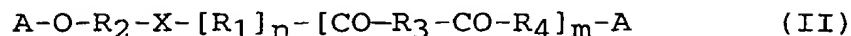
The object of the present invention is to provide low-cost and low-odor (meth)acrylic ester binders which can be used as reactive components for reactive acrylic systems, particularly for adhesives, coatings, floorings, mortars, and casting compounds with enhanced mechanical properties. Besides fulfilling the technical requirements of acrylic systems for industrial applications, the novel (meth)acrylate binders are, from the economical and ecological point of view, superior to already commercially available (meth)acrylic ester monomers.

Brief summary of the invention

The present invention provides low-cost and low-odor (meth)acrylic ester binders that are mixtures of oligomers, said oligomers comprising those of the following formula



and/or

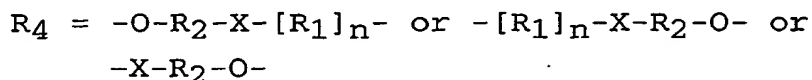


CO is carbonyl group

R_1 is a repetition unit of an aromatic polyester, in particular a repetition unit of PET and/or PEN,

R_2 is a divalent radical selected from the group consisting of optionally substituted linear and branched C_3 - C_{20} alkylen, cycloalkylen and aralkylen radicals, optionally substituted di-, tri- or tetraalkylen-ether radicals, and optionally substituted heterocyclic radicals, preferably such radicals derived from the alcohols or aminoalcohols mentioned above, whereby said substituents are preferably selected from the group consisting of hydroxy groups, ester group and alkyl group,

R_3 is a divalent radical selected from the group consisting of optionally OH or COOH substituted linear and branched aliphatic and aromatic and araliphatic radicals, in particular radicals with 3 to 14 C-atoms



R_5 is hydrogen or methyl group

X is -O- or -NH-, and

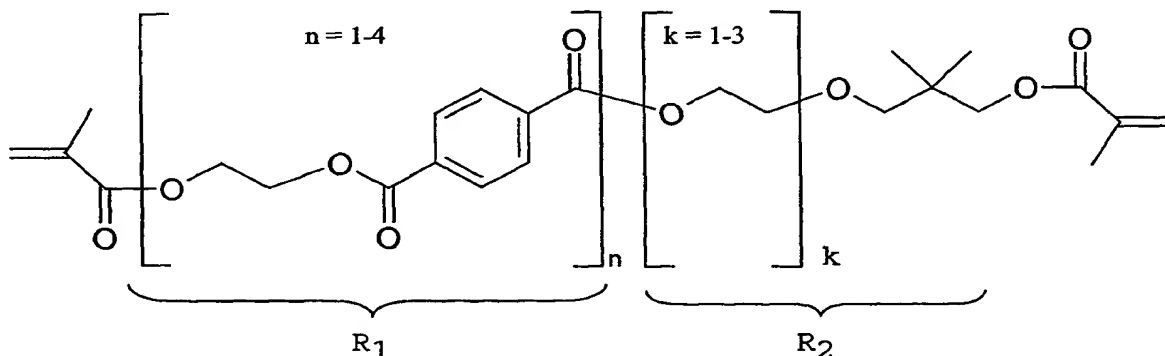
n is 1 to 4, and

m is 0 to 3.

$$\begin{array}{l} \text{A-O-R}_2\text{-X-A} \\ \text{A-[R}_1\text{]}_n\text{-O-R}_6 \\ \text{A-OH} \end{array}$$

10 R₆ is a linear or branched aliphatic or aromatic or araliphatic radical in particular a radical with 5 to 22 C-atoms.

A specific example of a non modified binder molecule is
15 shown below.



= repetition unit of PET = ethox. neopentyl glycol derived radical

25 Preferred binders are those that are obtain-
able from glycolyzed aromatic polyester such as polyeth-
ylene terephthalate (PET). These binders are suitable as
reactive components for reactive acrylic systems, more
specifically for adhesive, coating and flooring composi-
30 tions with:

- excellent mechanical properties, such as high tensile strength, high compressive strength and high scratch resistance.

- good weather and chemical resistance.

The (meth)acrylic ester binders of the present invention can be prepared by reacting polyesters containing free OH-groups with acrylic and/or methacrylic acid. The OH-terminated polyesters preferably are products of the reaction of high-molecular-weight aromatic polyesters such as PET with aromatic or aliphatic polyols and/or aminoalcohols.

The binders of the present invention - as they result from the reaction - are mixtures of molecules comprising PET fragments of generally 1 to 4 PET units, preferably 1 to 3 PET units.

The binders of the present invention can be present as such, or in compositions with other (meth)acrylates or ethylenically unsaturated vinyl monomers, or in formulations comprising at least one of the following further substances, namely catalysts, stabilizers, initiators, organic fillers, inorganic fillers, additives, toughening agents, adhesion promoters, defoaming agents, thickeners, thixotropic agents, plasticizers, wetting agents, wax compounds, cross-linking agents, inhibitors etc. Such additional substances are known to the skilled person and comprise e.g. as catalyst: N,N-dimethyl-p-toluidine, N-ethoxylated p-toluidine, N-alkylmorpholine; as inhibitor: hydroquinone, methylhydroquinone, t-butyl-p-cresol; as initiator: benzoylperoxide.

Advantages of the invention

30

The (meth)acrylate binders and binder compositions of the present invention have a low odor and can be radically cured to provide systems with exceptional mechanical properties. Tensile strength > 60 MPa can be reached, as well as high compressive strength, high scratch resistance, and excellent weather and chemical resistance. The (meth)acrylate binders of the present in-

vention posses low viscosity and good storage stability. The inventive binders can be synthesized by a process which overcomes the limitations of the known processes for the synthesis of acrylic ester monomers from

5 (meth)acrylic acid. In such process of the present invention, inexpensive raw materials such as recycled PET can be used and the production process is simple without expensive and time consuming reaction work up. The products are obtained in high yields and do not need further purification before use, which allows to obtain low-cost
10 (meth)acrylic esters. Another advantage of the invention is that the mechanical properties of the cured systems can be varied by chemical modification of the binder or binder composition, respectively. Therefore, the use of
15 external plasticizers which can diffuse out of the (meth)acrylate matrix, or of fillers which decrease the mechanical properties of the cured systems can be reduced and preferably avoided.

20
Detailed description of the invention

The (meth)acrylic ester oligomers of the present invention are preparable from high-molecular-weight
25 aromatic polyesters such as polyethylene naphthalate (PEN), polyethylene terephthalate (PET) or mixtures thereof. PET sources are either virgin or recycled PET, or waste PET from many sources such as beverage bottles, sheets, film and synthetic fibers.

30 The (meth)acrylic ester oligomers of the invention contain PET amounts within the range of about 10 to 80 wt.%; a more preferred range is from about 20 to 50 wt.%; especially preferred 30 to 40 wt.%. Preferably, PET should be flaked and washed before use, but the direct
35 use of waste beverage bottles is possible.

The also inventive synthesis of the (meth)acrylic ester oligomers is based on a two step pro-

cess, but the steps can be achieved consecutively in a one pot reaction. The steps of the process consist in:

(i) generation of hydroxy terminated binder precursor oligomers (OH-precursors) said generation involving a glycolysis or similar reaction of aromatic polyester(s) such as PET and

(ii) direct esterification of (meth)acrylic acid with said OH-precursors.

In the scope of the present invention, the product of step (i) that is further reacted in step (ii) is termed "hydroxy terminated binder precursor oligomers" or - shorter - "OH-precursors" since it usually is a mixture of OH-terminated oligomers. Said term comprises - dependent on whether or not a modification (chain extension) is performed - the "glycolysis" product (hydroxy terminated oligomer) or the reaction product of said "glycolysis" product with dicarboxylic acid(s) and/or anhydride(s). The term "glycolysis" for simplification is considered as also comprising the reaction with aminoalcohols.

The synthesis is now further described for the preferred polyester PET, however, it is also applicable to other aromatic polyesters.

(i) Generation of OH-terminated binder precursor oligomers (glycolysis of PET)

In accordance with the present invention, PET is first reacted with a polyol or polyol mixture in molar ratios of 0.2 (OH groups in polyol):1 (repetition unit in PET) to 2 (OH groups in polyol):1 (repetition unit in PET) in the presence of an esterification catalyst to yield low-molecular-weight polyesters containing free OH-groups. Particularly favorable are mixture in molar ratios of 0.8 (OH-groups in polyol) : 1 (repetition unit in PET) to 1.5 (OH groups in polyol) : 1 (repetition unit in PET), and even more favorable 1.1 (OH groups in polyol) :

1 (repetition unit in PET) to 1.3 (OH groups in polyol) :
1 (repetition unit in PET). The reaction requires nor-
mally 0.5 to 4 hours at temperatures between 210°C and
250°C, and it is preferably carried out under a N₂ atmos-
5 phere.

The polyols used for the glycolysis can be
aliphatic, cycloaliphatic, aromatic and/or heterocyclic
polyols, and are preferably selected from diols or
triols. Examples of suitable polyols are diethylene gly-
10 col, triethylene glycol, tetraethylene glycol, tripropyl-
ene glycol, 1,4-butanediol, 1,6-hexanediol, glycerin, di-
propylene glycol, neopentyl glycol, 2,2,4-trimethyl-1,3-
pentane diol, 1,2-propane glycol, 1,3-propane glycol,
1,3-butane glycol, 2,3-butane glycol, 1,5-pentanediol, 2-
15 methyl-1,5-pentanediol, 2-methyl-2-ethyl-1,3-propanediol,
bisphenol-A-ethoxylate, dodecahydro-bisphenol-A, dimeth-
ylol propionic acid, OH-terminated polybutadiene, trimeth-
ylolethane, 1,4-cyclohexanedimethanol, 1,2-cyclohexane-
dimethanol, 1,3-cyclohexanedimethanol, 1,4-bis(2-hydroxy-
20 ethoxy)cyclohexane, norbornylene glycol, 1,4-benzene-
diethanol, 2,4-dimethyl-2-ethylenehexane-1,3-diol, 2-
buten-1,4-diol, ethoxylated trimethylolpropane, trimeth-
ylolhexane, trimethylolpropane-monoallyether, 1,2,4-
butanetriol, dipentaerythritol, pentaerythrite, dicyclo-
25 pentadienedimethanol, ethoxylated neopentyl glycol, di-
methylhydantoin glycol, ethoxylated dimethylhydantoin
glycol, ethoxylated isocyanurate, and in particular di-
(2-hydroxyethyl)-5,5-dimethylhydantoin, 1,3-dimethylol-
5,5-dimethylhydantoin, tri-(2-hydroxyethyl)-isocyanurate,
30 and hydroxyalkyl isocyanurates. The PET-glycolysis can
also be achieved with a mixture of polyols or polyols and
aminoalcohols such as diethanolamine, triethanolamine and
triisopropanolamine. Instead of polyols, aminoalcohols or
mixtures of aminoalcohols can also be used. It is pre-
35 ferred that linear glycols such as diethylene glycols
etc. are used in combination with branched glycols to re-
duce the risk of crystallisation.

As catalyst, 0.1 wt.% to 2 wt.% of any esterification catalyst such as tin(II)caprylate, cobalt acetate, mangan(II)acetate, calcium hydroxide, calcium formiate, sodium hydroxide, barium hydroxide, and organic tin and titan catalysts can be added. Preferably, t-butyl ortho titanate is used.

(ii) Direct esterification of (meth)acrylic

10 acid

The OH-precursors obtainable by the glycolysis reaction (see above), and optionally the chain extension reaction (see below), are further reacted with (meth)acrylic acid (MAA) in molar ratios of 0.5 (acid group in MAA):1 (OH group in OH-precursor) to 2 (acid groups in MAA):1 (OH groups in OH-precursor) at temperatures from 90°C to 140°C to yield low-odor (meth)acrylic ester binders. The reaction is generally carried out in the presence of 0.1 wt.% to 2 wt.% of an esterification catalyst such as p-toluene sulfonic acid, methane sulfonic acid, sulfuric acid, boron trifluoride or any acid esterification catalyst. To prevent polymerization during reaction, a free-radical inhibitor such as hydroquinone, methyl hydroquinone, t-butyl p-cresol, phenothiazine and the like may be added in amounts ranging from 0.1 wt.% to 1 wt.% based on the weight of MAA. An inert solvent can be used to azeotrope the water resulting from the esterification reaction. Examples of solvents which are particularly useful are hexane, pentane, cyclopentane, cyclohexane, benzene, toluene, xylene or mixtures thereof. The preferred solvent is toluene. The reaction mixture may contain from about 5 wt.% to 30 wt.% of the selected solvent. The reaction is run for 4 to 5 hours or until no more water is formed.

35

Modifications

The properties of the cured acrylic systems can be varied by modification of the (meth)acrylic ester binders. Following the glycolysis step, the OH-terminated
5 low-molecular-weight polyesters can be reacted with at least one difunctional or multifunctional organic acid (and/or anhydride). The resultant polyester prepolymers yield, after direct esterification, methacrylic ester
10 binders which provide cured systems with special properties. Suitable organic acids (or anhydrides) are aliphatic and aromatic difunctional or multifunctional acids such as adipic acid, azelaic acid, phthalic acid or anhydride, isophthalic acid, dodecandicarboxylic acid, maleic acid or anhydride, trimellitic acid or anhydride and the
15 like.

The same procedure as outlined above can also be used with other starting materials such as PEN instead of PET, acrylic acid instead of methacrylic acid and aminoalcohols instead of polyols or part of polyols. Furthermore, in order to achieve specific features it is of
20 course also possible to use mixtures of starting materials such as mixtures of aromatic polyesters, mixtures of acrylic acid and methacrylic acid, mixtures of polyols or polyols and aminoalcohols, etc.

Curable acrylic systems for special applications can also be obtained by replacing a certain amount of the polyols by a monofunctional alcohol in the glycolysis step. The amount of monofunctional alcohol(s), or a mixture of monofunctional alcohol, depends on the desired
25 end use of the acrylic system. Preferably, the monofunctional alcohol(s) replaces 1 to about 90 mol% of the diol or polyol or aminoalcohol. Suitable alcohols include the C₅-C₂₂ linear and branched saturated and unsaturated alcohols including, for example, 4-methyl-1-pentanol,
30 hexanol, linoleoyl alcohol, benzyl alcohol, trimethylolpropane diallylether, allyl alcohol and nonanol. Other

useful alcohols include the OH-functional polyethers, polyesters, polyurethanes, polycaprolactones, etc.

5

Examples

Example 1

(without chemical modification)

10

475 g PET flakes from recycled beverage bottles, 520 g ethoxylated neopentyl glycol and 5 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and condenser. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the solution is allowed to cool until the reaction mixture has reached 130°C and then 365 g toluene, 460 g methacrylic acid containing 0.2 g phenothiazine, and 15 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and collected in the separator. The reaction is finished after about 4 hours, or when no more water is formed. Finally, the toluene is removed under reduced pressure. The mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 35 MPa, elongation at break of 9%, good scratch resistance and compressive strength, and excellent weather and chemical resistance.

Example 2

(without chemical modification)

475 g PET flakes from recycled beverage bottles, 520 g ethoxylated neopentyl glycol and 5 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and condenser. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the solution is allowed to cool until the reaction mixture has reached 130°C and then 459 g toluene, 836 g methacrylic acid containing 0.4 g phenothiazine, and 18 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and collected in the separator. The reaction is finished after about 4 hours or when no more water is formed. Finally, the toluene is removed under reduced pressure. The mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 65 MPa, elongation at break of 4%, good scratch resistance and compressive strength, and excellent weather and chemical resistance.

Example 3

(without chemical modification)

30

465 g PET flakes from recycled beverage bottles, a mixture of 300 g ethoxylated neopentyl glycol and 230 g nonanol N, and 5 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and condenser. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the solution is allowed to cool until the reaction

mixture has reached 130°C and then 454 g toluene, 815 g methacrylic acid containing 0.4 g phenothiazine, and 18 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and collected in the separator. The reaction is finished after about 4 hours or when no more water is formed. Finally, the toluene is removed under reduced pressure. The mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 30 MPa, elongation at break of 4%, good scratch resistance and compressive strength, and excellent weather and chemical resistance.

Example 4

(with chemical modification by reaction with phthalic acid anhydride)

395 g PET flakes from recycled beverage bottles, 440 g diethylene glycol and 5 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and an overhead condenser with receiver. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the reactor is allowed to cool to 200°C and 160 g phthalic acid anhydride are added. The mixture is kept at this temperature for about 2 hours and the water formed is collected in the receiver. Once no more water is formed, the solution is allowed to cool until the reaction mixture has reached 130°C, and then 378 g toluene, 513 g acrylic acid containing 0.3 g phenothiazine, and 15 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the

boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and collected in the separator. The reaction is finished after about 4 hours or when no more water is formed. Finally, the toluene is removed under reduced pressure. The mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 35 MPa, elongation at break of 6%, good scratch resistance and compressive strength, and excellent weather and chemical resistance.

Example 5

(with chemical modification by reaction with phthalic acid anhydride)

395 g PET flakes from recycled beverage bottles, 364 g diethylene glycol and 3 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and an overhead condenser with receiver. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the reactor is allowed to cool to 200°C and 237 g phthalic acid anhydride are added. The mixture is kept at this temperature for about 2 hours and the water formed is collected in the receiver. Once no more water is formed, the solution is allowed to cool until the reaction mixture has reached 130°C, and then 303 g toluene, 213 g methacrylic acid containing 0.1 g phenothiazine, and 12 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and collected in the separator. The reaction is finished after about 4 hours or when no more water is formed. Finally, the toluene is removed under reduced pressure. The

mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 12 MPa, elongation at break
5 of 30%, good scratch resistance and compressive strength, and excellent weather and chemical resistance.

Example 6

10 (with chemical modification by reaction with TMAS waste stream)

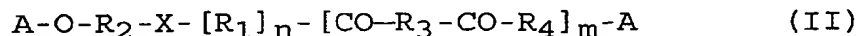
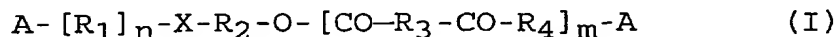
379 g PET flakes from recycled beverage bottles, 440 g diethylene glycol and 2 g t-butyl ortho titanate are charged into a reactor equipped with mechanical stirrer, temperature controller and an overhead condenser with receiver. The reaction mixture is heated for 2 hours at 240°C under N₂ atmosphere. Then, the reactor is allowed to cool to 200°C and 180 g TMAS (WS) are
15 added. The mixture is kept at this temperature for about 2 hours and the water formed is collected in the receiver. Once no more water is formed, the solution is allowed to cool until the reaction mixture has reached 130°C, and then 392 g toluene, 566 g methacrylic acid
20 containing 0.3 g phenothiazine, and 16 g p-toluene sulfonic acid are added. The reactor is further equipped with a water separator and the reaction is carried out at the boiling temperature of the mixture (about 130 °C). The water produced is distilled off with the solvent and
25 collected in the separator. The reaction is finished after about 4 hours or when no more water is formed. Finally, the toluene is removed under reduced pressure. The mixture obtained has low viscosity and is cured at room temperature with 2 wt.% benzoylperoxide as initiator and
30 0.5 wt.% dimethylaniline as catalyst to provide systems with tensile strength (TS) > 37 MPa, elongation at break
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of 8%, good scratch resistance and compressive strength,
and excellent weather and chemical resistance.

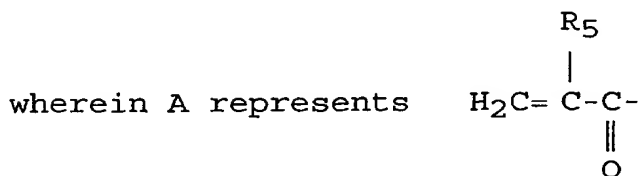
EPO - Munich
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01. Aug. 2000Claims

1. Methacrylate or acrylate binder comprising oligomers of the following formula (I) and/or (II)

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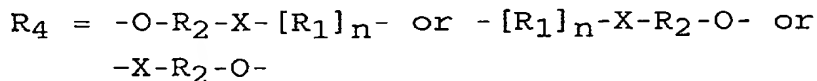
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CO is carbonyl group

R₁ is a repetition unit of an aromatic polyester, in particular a repetition unit of PET and/or PEN,

R₂ is a divalent radical selected from the group consisting of optionally substituted linear and branched C₃-C₂₀ alkylen, cycloalkylen and aralkylen radicals, optionally substituted dialkylenether, trialkylenether or tetraalkylenether radicals and optionally substituted heterocyclic radicals, whereby said substituents are preferably selected from the group consisting of hydroxy group, ester group and alkyl group,

R₃ is a divalent radical selected from the group consisting of optionally OH or COOH substituted linear and branched aliphatic and aromatic and araliphatic radicals, in particular radicals with 3 to 14 C-atoms,



R₅ is hydrogen or methyl group

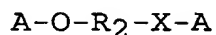
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X is -O- or -NH-, and

n is 1 to 4, and

m is 0 to 3.

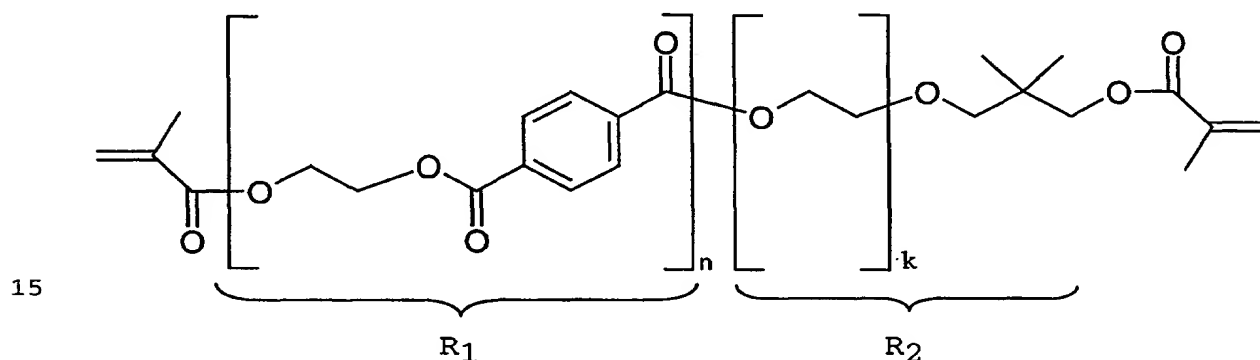
2. The binder of claim 1 that further comprises at least one compound selected from the group consisting of



wherein A, R_1 and R_2 are as defined above

R_6 is a linear or branched aliphatic or aromatic or araliphatic radical, in particular a radical with 5 to 22 C-atoms.

3. The binder of claim 1 or 2 that comprises the oligomer represented by



wherein R_1 is a repetition unit of PET
 R_2 is an ethoxylated neopentyl glycol derived radical
 n is 1 to 4, and
 k is 1 to 3.

4. The binder of anyone of the preceding claims that is obtainable by the steps of (i) generating hydroxy terminated binder precursor oligomers (OH-precursors) derived from at least one aromatic polyester, and (ii) reacting said OH-precursors of step (i) with methacrylic acid and/or acrylic acid to form a respective ester, whereby step (i) comprises reacting an aromatic polyester, or a mixture of aromatic polyesters with at least one polyol and/or at least one aminopolyol to generate hydroxy terminated oligomers.

5. The binder of anyone of the preceding claims, which is a methacrylate binder.

6. The binder of anyone of the preceding claims which is derived from PET.

5 7. The binder of anyone of claims 4 to 6
which is preparable using as polyol at least one diol, at
least one triol or a mixture thereof, preferably a polyol
selected from the group consisting of diethylene glycol,
ethoxylated neopentyl glycol, di-(2-hydroxyethyl)-5,5-
10 dimethylhydantoin, 1,3-dimethylol-5,5-dimethylhydantoin,
tri-(2-hydroxyethyl)-isocyanurate, hydroxyalkyl iso-
cyanurates, and mixtures thereof.

8. The binder of anyone of claims 4 to 7
which is preparable using a mixture of at least one
15 polyol and/or at least one aminoalcohol and at least one
monofunctional alcohol, preferably a monofunctional alco-
hol selected from the group consisting of C₅-C₂₂ linear
saturated alcohols, C₅-C₂₂ linear unsaturated alcohols,
C₅-C₂₂ branched saturated alcohols, C₅-C₂₂ branched unsatu-
20 rated alcohols, and mixtures thereof, more preferably a
monofunctional alcohol selected from the group consisting
of 4-methyl-1-pentanol, hexanol, linoyleyl alcohol, benzyl
alcohol, trimethylolpropane diallylether, allyl alcohol,
nonanol, and mixtures thereof.

25 9. The binder of claim 7 or 8 wherein the al-
cohol is selected from monohydroxy functional or dihy-
droxy functional polymers or oligomers selected from the
group consisting of polyethers, polyesters, polyure-
thanes, polycaprolactones or mixtures thereof.

30 10. The binder of anyone of claims 4 to 9
wherein said OH-precursors of step (i) that are further
reacted in step (ii) are identical with said hydroxy ter-
minated oligomers.

11. The binder of anyone of claims 4 to 9,
35 wherein said OH-precursors of step (i) that are further
reacted in step (ii) are obtainable by further reacting
said hydroxy terminated oligomers with at least one poly-

carboxylic acid and/or at least one polycarboxylic anhydride.

12. The binder of claim 11, wherein the polycarboxylic acid is a dicarboxylic acid or an anhydride of a dicarboxylic acid, preferably a dicarboxylic acid or anhydride selected from the group consisting of adipic acid, azelaic acid, phthalic acid or anhydride, isophthalic acid, dodecandicarboxylic acid, maleic acid or anhydride, trimellitic acid or anhydride and the like.

13. Method for the production of a binder of anyone of claims 4 to 12 comprising the steps of (i) generating OH-precursors from at least one aromatic polyester, and (ii) reacting said OH-precursors of step (i) with methacrylic acid and/or acrylic acid to form a respective ester, whereby step (i) comprises reacting an aromatic polyester, or a mixture of aromatic polyesters with at least one polyol and/or at least one aminopolyol to generate hydroxy terminated oligomers.

14. The method of claim 13, wherein step (i) furthermore comprises reacting said hydroxy terminated oligomers with at least one polycarboxylic acid and/or at least one polycarboxylic anhydride to get said OH-precursors.

15. A composition of binders comprising binders of one of claims 1 to 12 and at least one other (meth)acrylate and/or ethylenically unsaturated vinyl monomer.

16. A formulation comprising a binder of anyone of claims 1 to 12 or a composition of claim 15 and at least one further substance selected from the group consisting of initiators, catalysts, stabilizer, binders different from a (meth)acrylate binder or ethylenically unsaturated vinyl monomer, fillers and additives.

17. The formulation of claim 16 that is an adhesive formulation, a coating formulation, a mortar formulation, a casting compound formulation or a flooring formulation.

18. Use of a binder of anyone of claims 1 to 14, or of a composition of claim 15 or of a formulation of claim 16 or 17 as or in a adhesive, coating, flooring, mortar, or casting compound.

5 19. Method for producing a joint, coating or flooring, characterized in that a binder of anyone of claims 1 to 12 or a composition of claim 15 or a formulation of claim 16 or 17 is applied on at least one substrate such that wetting and adhesion is achieved.

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EPO - Munich
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01. Aug. 2000**Abstract**

Described are methacrylate or acrylate bind-
ers e.g. obtainable by the steps of (i) generating OH-
5 precursors from at least one aromatic polyester, and (ii)
reacting said OH-precursors of step (i) with methacrylic
acid and/or acrylic acid to form a respective ester,
whereby step (i) comprises reacting an aromatic polyes-
ter, or a mixture of aromatic polyesters with at least
10 one polyol and/or at least one aminopolyol to generate
hydroxy terminated oligomers.

Optionally, a modified product can be ob-
tained by performing a further reaction in step (i),
namely by reacting said hydroxy terminated oligomer with
15 at least one polycarboxylic acid and/or at least one
polycarboxylic anhydride to generate said hydroxy termi-
nated binder precursor oligomer.

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